

## THE BEHAVIOUR OF MAGNETITE AS RETAINING COVER IN THE SLUICE BOXES

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**ABSTRACT** A number of experiments, in a magnetic sluice with rectangular box cross section dimensioned 1200/200/100 mm were carried out. The sluice box was placed over a magnetic unit in which permanent magnets were incorporated to create a magnetic field over the sluice bottom. The magnetic field strength increased along the direction of flow of the treated suspension. The investigations were carried out by using a model suspension for determination of the possibilities of fine cassiterite recovery by detention in magnetite flocs. Detained magnetic fraction like dendrite flocs of magnetite create a sluice coating with high detention ability. The coarsest aggregates from detained magnetic fraction, mainly over the strong magnetic field zones, permits a heavy mineral concentration to take place within a form similar to classical sluices riffles. The retention of heavies can be achieved by means of fixing within the volume of magnetite flocs. The role of the hydrodynamics conditions was observed in a search for better recovery. The experimental results indicate that the optimal (one) or maximum recovery depends on the relationship between % solids and flow rate. The hydrodynamics conditions at lower flow-rates and lower pulp solids were the most favourable (60% recovery) but the heavy particle recovery slightly (50%) in hydrodynamic conditions of 10 l/min and 10% pulp-solids, but the kinetics of the process was considerably better. 50-60% recovery of fine heavy particles with a ratio of concentration 20 shows that the magnetite flocs could successfully be employed as captive coatings in sluice boxes.

### INTRODUCTION

Preliminary investigations on the prospects of a magnetic bottom sluice having 600 mm length were carried out to recover placer gold from construction sand. The feasibility of the method was confirmed by the test results indicating 20% stage recovery of free gold (Patcheff, S. Stoev 1989). By means of fractional analysis it was established that gold particles under 100 μm predominate in the yielded concentrate. The best results stipulated by a visual observation militated the necessity for a detailed study of the conditions for heavy mineral concentration in a magnetite cover.

The experiments are carried out in a 1200 mm long and 200 mm width sluice. The sluice is laid over the magnetic unit in which permanent magnets are incorporated to the location of bottom magnetic field the magnetisation of which following pulp detention is increased. Detained magnetic fraction like dendrite lines create a soil coating with high contact ability on the sluice bottom. The coarsest aggregates of the detained magnetite fraction in the over the strong magnetic field zones permit heavy particles to concentrate in the sluice like elutriated slimes.

Except this, heavies can be fixed also within the volume of the magnetite flocs originating from the pulp bearing magnetite. The ability of the magnetic capture coating to produce various concentrate zones characterised by a definite retention capability for particles of size and shape indicates that there is a possibility to both detain fine and coarse heavy particles. The magnetic fraction contained in the flowing continuous suspension permit over coating captured heavy particles to be packed into magnetite flocs and keep high contact ability on the capture coating. The process of deposition by packing is limited by the thickness of the fixed layer along the bottom magnetic fraction. Thickening causes a decrease of the magnetic force acting on the surface layer of particles. From the point of view of the hydrodynamic force, pulp flow can preferentially lift the fine particles on the sluice bottom. On hydrodynamic forces die especially in the case of packing of nonmagnetic particles in the sluice and may continue in some of the following unsaturated zones.

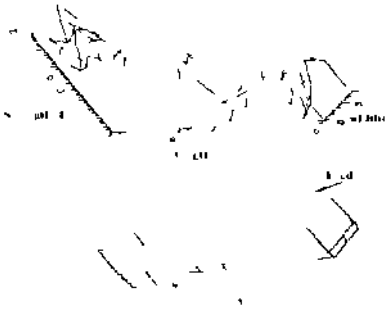


Figure 1 Magnet held/ones

A partial mechanical detachment of the captured magnetite particles from the surface of magnetite aggregates by the flowing suspension and the eventual filling of then places by low coercive magnetite particles is possible. The exchange of magnetic particles between the suspension and concentrated coating bungs about a state of high concentration as regards to the relatively slowly moving particles in the bottom layer.

The results of this experiment give a broad idea of the possibilities and efficiency of the method and could serve for the definition of the technological conditions.

## 2.1. EXPERIMENTAL METHOD

The experiment was carried out in a pilot scale equipment consisting of a pulp mixer, sluice box drainage system and hoses (Figure 2). The sluice slope was 1:1. In all tests the density of the pulp of approximately 1.2 is maintained by weight 40% within the mixture. The flow rate and pulp solids concentration were varied by means of addition of water in the sluice. The sluice was moved vertically.

The solid particles in the model suspension consisted of iron filings and at 100-200 micrometers in diameter in the cassiterite is heavy particles (PbO<sub>2</sub> with size up to 30mm).

During the experiment the amount of settling on the sluice bottom was moved by the sluice, the bottom magnetic unit. The concentration of the collected material and divided into non-magnetic

size ranges by screening. After that each range underwent magnetic separation.

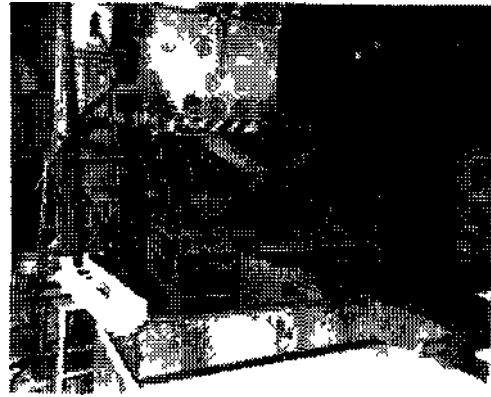


Figure 2 Experimental equipment

The magnetic fraction with a size between 100-200 micrometers was returned for use again as model of working magnetic traction and the nonmagnetic fraction with size below 40 micrometers is analysed for Sn. The tailing from the test process was collected, the water was decanted off and the sand fraction was used again (Figure 3).

## 3. RESULTS AND DISCUSSION

Before the main technological characteristics of the concentration with a magnetic sluice to be studied, some preliminary experiments were carried out for determining the working cycle duration and the optimum content of magnetic fraction in the suspension. According to the results of the previous experiments a constant 0.7% grade of magnetite was established in all tests. The clean up cycle depended mainly on the concentrate volume retained on the sluice bottom.

The curves drawn at Figure 4 show the dependence of cassiterite recovery vs pulp solids and flow rate. It is obvious that there is a trend obtained from the experimental results from which it is possible to make a conclusion that the recovery of cassiterite is maximum at low flow rates and low pulp solids. Similar final results were obtained when the flow rates became higher and pulp solids increase. From the results presented it is possible to assume that a satisfactory cassiterite recovery could be obtained if there is a synchronous change in the flow rates and pulp solids (B. P. D. R. Helincht, 1992).

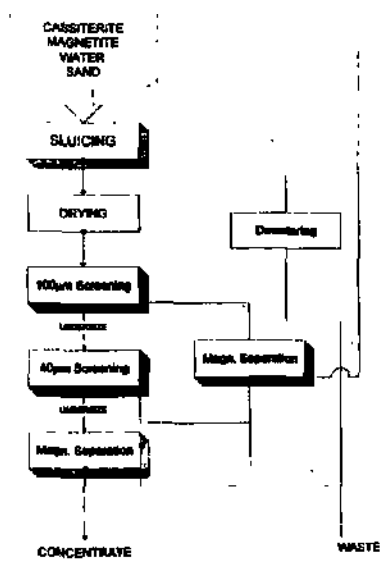


Figure 3. Experimental flowsheet

From the results presented at Figure 5, it is possible to observe the dependence of magnetite content in the retained concentrate vs on pulp solids and flow rate changes. The trend of the presented curves is very similar to the curves explained at Figure 4, which confirms a common trend of dependence of magnetite content (recovery) vs synchronous variations in pulp solids and flow rate. The analysis of the test results indicates the functional dependence of the recovery of fine cassiterite upon the solids content and the flow rate of the treated suspension. At lower values of these parameters, the recovery is higher (up to 69 %) unlike the cases of high flow rate at low retained density or high density at low flow rate (up to 15% recovery). In order to achieve maximum recovery at very high flow rates of the treated pulp it is necessary to increase the solids content of the suspension or vice versa. Therefore an optimal result may be achieved at different values of the flow rates and respective solid phase content

The test results indicate that could be assumed that the recovery of heavy fine particles by means of a short magnetic sluice is function of the relationship between pulp solids and flow rate -  $R=f[k(Q,T)]$ , where ;

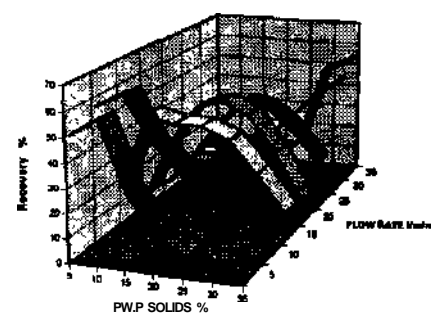


Figure 4. Recovery of Cassiterite v/s pulp solids and flow rate.

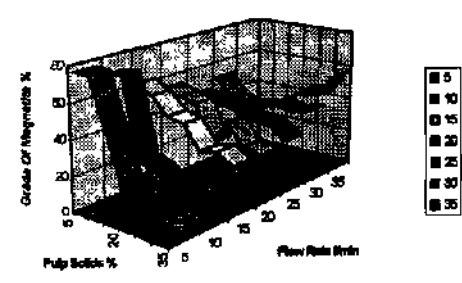


Figure 5. Grade of Magnetite in the concentrate v/s pulp solids and flow rate.

- R- recovery
- Q- flow rate
- T- pulp solids
- k- coefficient of sluice dimensions

The functional dependence of the cassiterite recovery vs pulp solids and flow rate relationship (in natural logarithmic scale) is presented at Figure 6. Curve 1 at the Figure 6 presents the trend of distribution of experimental data, while Curve 2 presents the fitted distribution with a coefficient of reliability of 0.85. Curve 2 obtained possess a Gauss distribution form of the dependence of cassiterite recovery on Ln Q/T parameters playing the main role in the process. The process could be described by the following equation:

$$R = A \cdot e^{b \ln(k \frac{Q}{I})^2}$$

where A and b are the coefficients of the equation with values of

$$\begin{aligned} A &= 39.1067 \\ b &= -0.7925 \\ k &= 1 \end{aligned}$$

and the equation finally results in the following form

$$R = 39.1067 \cdot e^{-0.7925 \ln(\frac{Q}{I})^2}$$

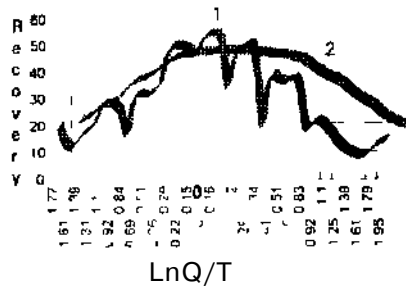


Figure 1. Dependence of the cassiterite recovery on pulp density and rate relationship

#### 4 CONCLUSION

The experimentally determined dependence of the process of concentration of fine heavy particles by means of magnetic sluice yields a model of hypothetical optimal areas of better performance as a function of Q/T relationship, which could be successfully applied for all types of magnetic sluices.

The process of packing of the valuable components by magnetite fines has a practical significance in view of cost-effective concentration of fine heavy particles.

From the processing point of view it is more feasible to maintain the process with higher flow rate and high pulp density due to the increased capacity.

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